

Amendments to the Specification:

Please amend the specification as follows:

On page 7, please replace the paragraph that starts at line 13 and ends at line 20 with the following amended paragraph:

Figures 2, 4, 6 and 8 are plots of differential scanning calorimetry (DSC) for fibers in various of the examples described later in this specification (a particular form of DSC, known as the Modulated MODULATED DSCTM techniques, using an instrument supplied by TA Instruments, Inc of New Castle, DE, was conducted, and provides additional information): Figures 2 and 4 are the DSC plot for fiber in the web of Example 31; Figure 2 is a plot for the fiber before annealing, and Figure 4 is a plot for the fiber after annealing; Figure 6 is the DSC plot for fiber in the web of Example 10; and Figure 8 is the DSC plot for fiber in the web of Example 22.

On page 8, please replace the paragraph that starts on line 30 and ends on page 9 at line 16 with the following amended paragraph:

In general, dimensionally stable webs of the invention are achieved by controlling a number of the parameters of the meltblowing process. Two such parameters are the temperature of the polymer in the meltblowing die, i.e., the temperature of the molten polymer in the extruder 13 and die cavity 12, and the temperature of the gas, generally air, blown through the slots 15 onto the polymer extrudate. By heating the polymer in the extruder and die cavity to a temperature lower than conventionally used in meltblowing, and thereby lowering the temperature of the polymer as it exits the die orifices 11, the frost line (the point at which the molten extrudate freezes or solidifies, i.e., changes from a molten condition to a solid condition) is brought closer to the die. The result is that during attenuation of the extrudate into fibers the polymer chains tend to be straightened and oriented and to retain a substantial portion of that orientation. A portion of the straightened and oriented polymer chains ~~[[are]]~~ is still amorphous ("amorphous orientation," in which the orientation is not sufficient to induce formation of a crystalline structure). But another portion of the polymer chains experiences sufficient stress, the "critical stress," to align the polymer chains sufficiently to facilitate a chain-extended

crystalline structure. This chain-extended crystalline structure, also called strain-induced crystallization, contributes to the unique properties of meltblown fibers of the invention.

On page 10, please replace the paragraphs starting at line 15 and ending on page 11 at line 3 and replace with the following amended paragraphs:

A different parameter useful in achieving dimensionally stable webs of the invention is the velocity of the primary air blown from the slots 15. The higher the velocity of that air, the greater the force applied to the extrudate, which tends to orient the polymer chains within the extrudate. Higher velocity is achieved by increasing the pressure in the supply leading to the slots 15, thus increasing the volume of air or other gas blown through the slots 15. Through analysis of exemplary processes of the invention, we have found that the primary air (or other gas) preferably has a velocity of at least 100 meters per second, and more preferably at least 150 meters per second. This velocity in feet/sec is determined by the following equation where Q is the SCFM of air flow used, P is the pressure in psi at the die exit and is assumed to have a value of 0 psi, t is the air temperature in degrees F, and a is the combined area of the slots 15 in square feet.

$$\text{Air velocity} = \left[\frac{Q}{\left(\frac{P + 1.03529 \cdot 10^5}{1.03529 \cdot 10^5} \right) \left(\frac{295.1k}{t + 273k} \right)} \right]^{1/60} \cdot 1/a$$

For SI units (where distances are in meters, so velocity is in meters/second, area is in square meters and Q is in SCMM; pressure is in pascals, and temperature is in degrees C), the equation is:

A different parameter useful in achieving dimensionally stable webs of the invention is the velocity of the primary air blown from the slots 15. The higher the velocity of that air, the

$$\text{Air velocity} = \left[\frac{Q}{\left(\frac{P + 14.7}{14.7} \right) \left(\frac{530}{t + 460} \right)} \right]^{1/60} \cdot 1/a$$

greater the force applied to the extrudate, which tends to orient the polymer chains within the extrudate. Higher velocity is achieved by increasing the pressure in the supply leading to the slots 15, thus increasing the volume of air or other gas blown through the slots 15. Through analysis of exemplary processes of the invention, we have found that the primary air (or other gas) preferably has a velocity of at least 100 meters per second, and more preferably at least 150 meters per second. This velocity in feet/sec is determined by the following equation where Q is the SCFM of air flow used, P is the pressure in psi at the die exit and is assumed to have a value of 0 psi, t is the air temperature

in degrees F, and a is the combined area of the slots 15 in square feet,

For SI units (where distances are in meters, so velocity is in meters/second, area is in

$$\text{Air velocity} = \left[\frac{Q}{\left(\frac{P + 14.7}{14.7} \right) \left(\frac{530}{t + 460} \right)} \right] \frac{1}{60} \cdot \frac{1}{a}$$

square meters and Q is in SCMM; pressure is in pascals, and temperature is in degrees C), the equation is:

$$\text{Air velocity} = \left[\frac{Q}{\left(\frac{P + 1.03529 \cdot 10^5}{1.03529 \cdot 10^5} \right) \left(\frac{295.1k}{t + 273k} \right)} \right] \frac{1}{60} \cdot \frac{1}{a}$$

On page 11, please delete the formula that appears at line 28. The formula to be deleted is shown below:

$$\text{Air velocity} = \left[\frac{Q}{\left(\frac{P + 14.7}{14.7} \right) \left(\frac{530}{t + 460} \right)} \right]^{1/60} \cdot \frac{1}{a}$$

On page 16, please replace the paragraph that starts on line 21 and ends on page 17 at line 4 with the following amended paragraph:

A differential scanning calorimetry plot, attached as Figure 6, was generated for a representative fiber web of Example 10 using a ~~Modulated~~ **MODULATED** DSC™ technique and system (Model 2920 supplied by TA Instruments Inc, New Castle, DE), and using a heating rate of 4 degrees C/minute, a perturbation amplitude of plus-or-minus 0.636 degrees C and a period of 60 seconds. A WAXS diagram for fibers of Example 10, attached as Figure 7, was collected by use of a Bruker microdiffractometer, copper K_α radiation, and Hi-STAR 2D position sensitive detector registry of the scattered radiation (supplied by Bruker AXS, Inc, Madison, WI). The diffractometer was fitted with a 300 micron collimator and graphite incident beam monochromator. The X-ray generator consisted of a rotating anode source using a copper target operated at settings of 50 kV and 100 mA. Data were collected using a transmission geometry for 60 minutes with the detector centered at 0 degrees (2θ) at a sample to detector distance of 6.0 cm. Samples were mounted so as to place the fiber direction in the vertical. The 2D detector data were corrected for detector sensitivity and spatial irregularities using the Bruker GADDS data analysis software.

On page 21, please replace the paragraph, which appears between Table 4 and Table 5 with the following amended paragraph:

A series of webs of the invention were prepared from PET having an intrinsic viscosity of 0.50 using a meltblown die as described in Examples 1-17. The processing temperature for the PET polymer was set to 273°C and the temperature of the air passing through the slot 15 was set to 258°C. The collector was set as described in Examples 1-17 to produce a web of about 260 grams/square meter. The webs were annealed at 160 degrees C for 5 minutes and then measured for tensile properties using tests as described in ASTM D 5034 (maximum load, in pounds-force) in the machine direction and using an ~~Instron~~INSTRONTM Tensile Tester (Model 4302) at a separation rate of 12 inches/minute (30.48 cm/minute). The jaw gap was set to 0.25 inches (0.64 cm) and the sample width was 1.0 inch (2.54 cm). The test was based on 5 samples and the averaged results are reported in Table 5.